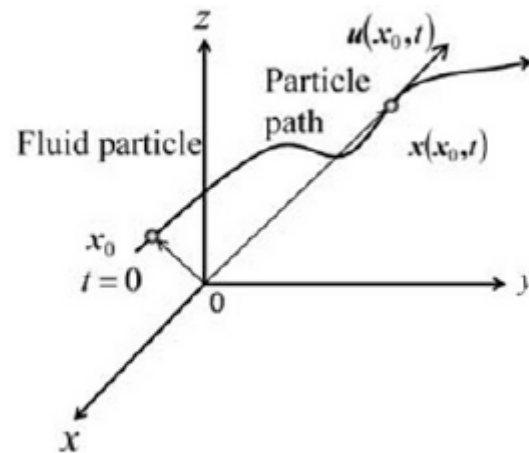


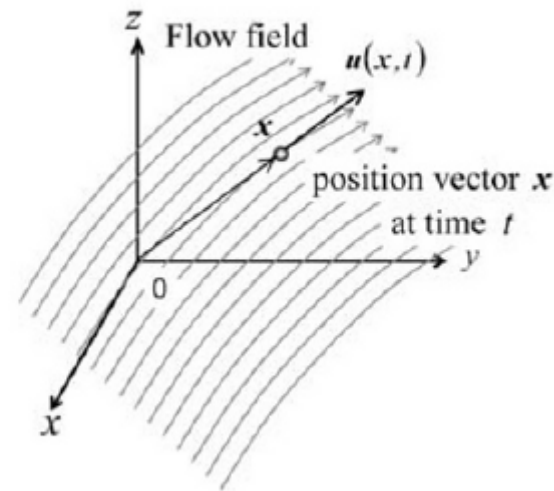
# Motion of a Fluid

1

(a) Lagrangian specification



(b) Eulerian specification



Description of fluid motion

- The motion of a fluid can be determined, when the velocity at every point of the space is occupied by fluid motion.
- Therefore, to express the velocity with independent variables, there are two distinct methods available,
  - (i) Lagrangian method ; (ii) Eulerian method.

# Motion of a Fluid

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2

- Lagrangian method
- traces the motion of a fluid particle in space with time
- The position vector  $\mathbf{x}$  of the fluid particle, considering a motion relative to a given frame of reference at time  $t$ , can be expressed as

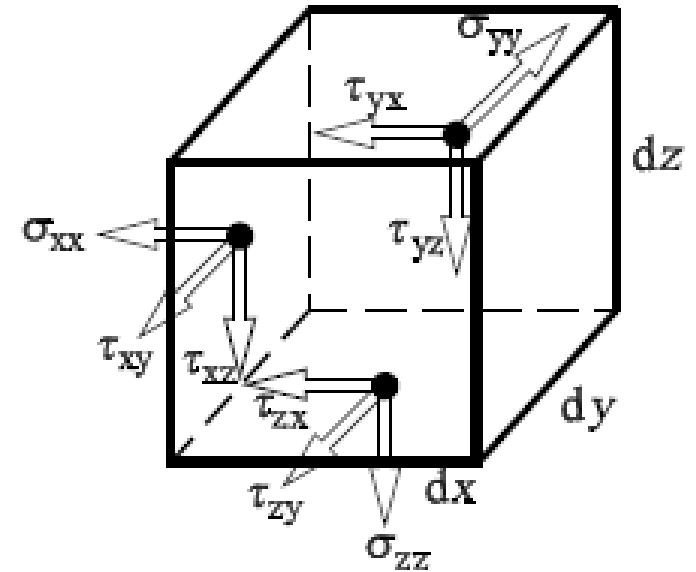
$$\mathbf{x} = \mathbf{x}(\mathbf{x}_0, t)$$

- where  $\mathbf{x}_0$  and  $t$  are independent parameters, and  $\mathbf{x}_0$  is the original position at  $t = 0$
- The velocity  $\mathbf{u}$  and acceleration  $\mathbf{a}$  at time  $t$
- can be written similarly as

(ii) Eulerian method.  $\mathbf{u} = \mathbf{u}(\mathbf{x}_0, t) = \frac{\partial \mathbf{x}}{\partial t}$        $\mathbf{a} = \mathbf{a}(\mathbf{x}_0, t) = \frac{\partial \mathbf{u}}{\partial t}$

# Stresses in Fluid: Viscous stress

- The *general theory of liquid friction* tells us that when the shape of a single liquid element is changed, stresses arise that are similar to those of elastic bodies.
- The difference lies in the fact that these stresses are not proportional to the changes of shape, but rather to the **velocities** of the changes of shape.
- The equations for the nine stress components (three each on the three surfaces perpendicular to the coordinate axes (see the Figure)) therefore read (for **Newtonian and incompressible fluid**)



Normal and shear stress at volume element  $dV = dx \cdot dy \cdot dz$

$$\sigma_{xx} = 2 \cdot \mu \cdot \frac{\partial u}{\partial x}, \quad \tau_{xy} = \tau_{yx} = \mu \cdot \left( \frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right),$$

$$\sigma_{yy} = 2 \cdot \mu \cdot \frac{\partial v}{\partial y}, \quad \tau_{yz} = \tau_{zy} = \mu \cdot \left( \frac{\partial v}{\partial z} + \frac{\partial w}{\partial y} \right),$$

$$\sigma_{zz} = 2 \cdot \mu \cdot \frac{\partial w}{\partial z}, \quad \tau_{zx} = \tau_{xz} = \mu \cdot \left( \frac{\partial w}{\partial x} + \frac{\partial u}{\partial z} \right).$$

# Stresses in Fluid: Viscous stress

- For *general Newtonian fluids*.

$$\sigma_{xx} = 2 \cdot \mu \cdot \frac{\partial u}{\partial x} - \frac{2}{3} \cdot \mu \cdot \left( \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} \right),$$

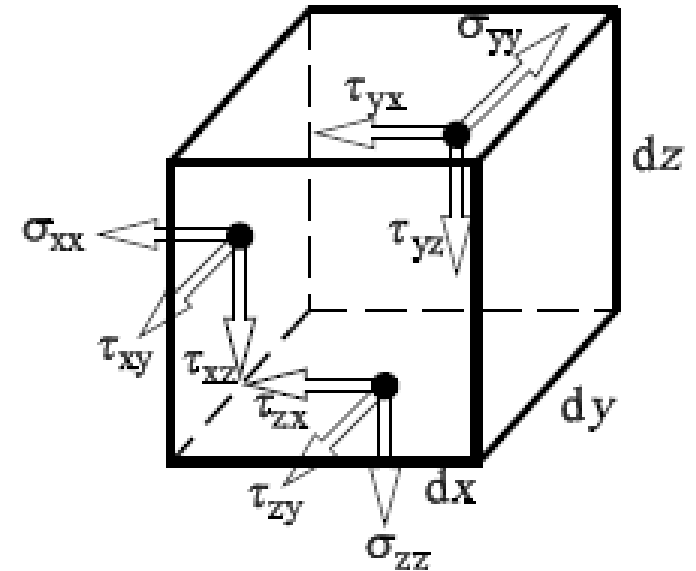
$$\sigma_{yy} = 2 \cdot \mu \cdot \frac{\partial v}{\partial y} - \frac{2}{3} \cdot \mu \cdot \left( \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} \right),$$

$$\sigma_{zz} = 2 \cdot \mu \cdot \frac{\partial w}{\partial z} - \frac{2}{3} \cdot \mu \cdot \left( \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} \right),$$

$$\tau_{yx} = \tau_{xy} = \mu \cdot \left( \frac{\partial v}{\partial x} + \frac{\partial u}{\partial y} \right),$$

$$\tau_{zx} = \tau_{xz} = \mu \cdot \left( \frac{\partial u}{\partial z} + \frac{\partial w}{\partial x} \right),$$

$$\tau_{yz} = \tau_{zy} = \mu \cdot \left( \frac{\partial w}{\partial y} + \frac{\partial v}{\partial z} \right),$$



Normal and shear stress at volume element  $dV = dx \cdot dy \cdot dz$

# Continuity Equation

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5

- In general, the conservation of mass at a volume element may be formulated as follows:

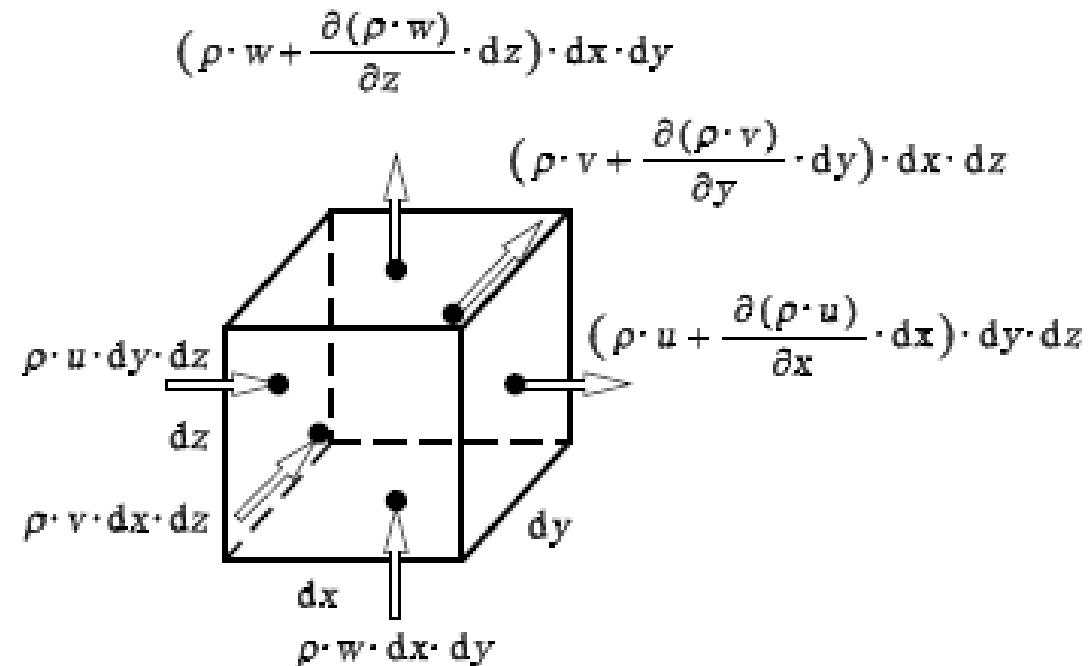
*The rate of change of mass in a volume element*

*=  $\sum$  the mass fluxes into the volume element*

*-  $\sum$  the mass fluxes out of the volume element.*

# Continuity Equation

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Mass fluxes entering and exiting the volume element  $dV$